8080D
Ultrafiltration Element

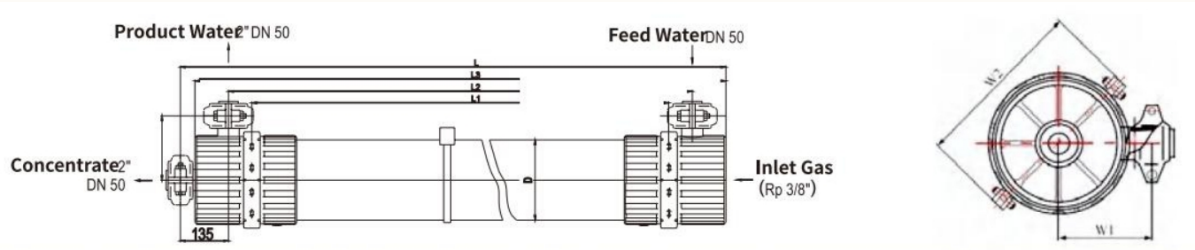
Overview

This product uses high-strength, chemical-resistant PVDF hollow fiber membranes to ensure long service life and reliable operation. It effectively removes bacteria, viruses, and particles (including colloids) to protect downstream equipment such as RO systems. Its strong chemical resistance extends membrane lifespan, and its easy-to-clean and wettable properties maintain long-term performance. The external pressure structure withstands higher feed suspended solids, reducing pretreatment requirements.

Specification

Application	Material	Effective Membrane Surface Area, $m^2(ft^2)$	Membrane Module Capacity, L(gal)	FWeight (Empty/Filled with Water), kg(lb)
NSF/ANSI61 Drinking Water	**PDVF Hollow Fiber**	**77(829)**	**39(10.3)**	**61/100(135/220)**

Size



L, inch (mm)	L1, inch (mm)	L2, inch (mm)	L3, inch (mm)	D, inch (mm)	W1, inch (mm)	W2, inch (mm)
92.9±0.1 (2360±3)	78.7(2000)	83.9±0.1 (2130±3)	91.3±0.1 (2320±3)	Φ8.9(Φ225)	7.1(180)	13.5(342)

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Operating Parameters

Filtration Flux (at 25°C), L/m²/hr	40-90
Flow Rate Range, m³/hr	3.1-6.9
pH (Operating)	2-11
Temperature, °C	1-40
Max. Feed Water Pressure for Membrane Module (@20°C), bar	6.25
Max. Operating Transmembrane Pressure Difference, bar	2.1
Max. Air Scouring Flow Rate, Nm³/hr	12
Max. Backwash Pressure, bar	2.5
Max. NaClO Tolerance Concentration, mg/L	2,000
Max. Suspended Solids Tolerance Concentration, mg/L	100
Turbidity (Max.), NTU	300
Particle Size (Max.), μm	300
Flow Configuration	Outside-in, dead-end filtration
Expected Post-filtration Turbidity, NTU	⩽0.1
Expected Filtration Sludge Density Index (SDI)	⩽2.5

Operation:
During start-up, shut-down, cleaning, or other operational processes, it is important to prevent damage to the membrane elements caused by sudden pressure changes. Prior to start-up, the UF system should be flushed to remove the transport protection fluid and expel any residual air. During the initial operation, the equipment should be started manually, with the initial permeate flow rate controlled at 60% of the designed capacity. The permeate produced during the first run should be discharged completely; specific requirements may vary depending on the application.

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